Combustion of fossil fuels currently provides around 80% of the traded energy generally in industrialized economies and will continue to be a major energy source for the foreseeable future. Simultaneously, the traditional combustion has been producing heavy emissions of carbon dioxide (CO₂), nitric oxides (NOₓ) and fine particles (PM), and hence posing serious threats to our human life. An urgent action must be taken to reduce these emissions!

Establishment of MILD combustion and its characteristics have been widely studied in recent years [7–14]. Weber et al. [7] examined the combustion characteristics of natural gas, heavy and light oils, and coal in highly preheated air in a semi-industrial scale furnace, finding that MILD combustion can be realized over a wide temperature of reactants and the reduced temperature rise in the combustion process [1]. Practically, internal or external exhaust gas recirculation (EGR) is commonly used to preheat incoming reactants and thus realize MILD combustion [4,5]. In the external EGR system, the recuperator and regenerator are usually used to absorb the waste heat of the flue gas and preheat the inlet reactants [3]. Comparing to traditional combustion processes, the thermal efficiency is higher in MILD combustion. Two reasons account for this. Firstly, the low peak temperature and the uniform furnace temperature reduce the irreversible heat loss in the combustion and heat transfer processes [6]. Secondly, the uniform temperature field and high flow speed in the furnace enhance the heat transfer, especially the radiative one [3]. Moreover, because the reactant temperature prior to the main reaction zone is higher than Tₚ and the temperature rise is low, MILD combustion is more stable and produces much lower noise than traditional combustion [1].

1. Introduction

MILD combustion versus conventional bluff-body flame of a premixed CH₄/air jet in hot coflow

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ABSTRACT

The present work is to investigate the MILD (moderate and intense low-oxygen dilution) combustion of a premixed methane jet in hot coflow against its conventional counterpart, i.e., a typical bluff-body flame, under identical inlet and boundary conditions. This paper demonstrates that the MILD combustion develops as a stable ‘flame’ lifting far downstream from the nozzle while the conventional flame evolves immediately behind the bluff body. More specifically, all chemical reactions are found to occur far more slowly over a greatly larger reaction zone for the MILD combustion than for the conventional one. Also, for the MILD combustion, the laminar flame speed (S_l) is very small, far below the local flow speed (U), whereas chemical and mixing times are compatible so that the Damkohler number Da ~1.0. In contrast, the conventional combustion takes place with S_l ≥ U and Da = 10–1000. Moreover, the MILD combustion eventually emits little NOx, only less than 3% of the emission from the conventional counterpart. Fundamentally, the MILD combustion produces the NOx emission mainly through the N₂O-intermediate and NNH routes while the thermal NOx mechanism dominates the conventional flame. In addition, this paper provides a comprehensive explanation to each of the above differences.

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**Nomenclature**

**Symbols**
- \( d \): diameter of the premixed jet nozzle (mm)
- \( Da \): Damköhler number
- \( EINO \): NO emission index (g-NO/kg-fuel)
- \( FL \): flame index
- \( I_0 \): integral length scale (m)
- \( I_k \): Kolmogorov length scale (m)
- \( m_{NOx} \): NOx mass flux (kg/s)
- \( P \): thermal power rate (kW)
- \( Re \): jet exit Reynolds number
- \( Re_t \): turbulent Reynolds number
- \( S_L \): laminar flame speed (m/s)
- \( T_{ai} \): auto-ignition temperature (K)
- \( T_c \): inlet temperature of the coflow (K)
- \( T_j \): inlet temperature of the premixed jet (K)
- \(<T>_F\): Favre-averaged temperature (K)
- \(<T>_{max}\): maximum Favre-averaged temperature in the whole computational domain (K)
- \( T' \): root-mean-squared temperature (K)
- \( U_c \): coflow velocity (m/s)
- \( U_e \): jet exit velocity (m/s)
- \( u'_x \): axial velocity (m/s)
- \( VR \): reaction zone volume (m³)
- \( VR,P \): volume of the well-premixed reaction region (m³)
- \( X_i \): mole-fraction of species \( i \) in the premixed jet or coflow
- \( Y_i \): mass fraction of species \( i \) after reaction
- \( <Y_i>_F\): Favre-averaged mass fraction of species \( i \) after reaction
- \( <Y_i>_{max}\): maximum Favre-averaged mass fraction of species \( i \) in the whole computational domain
- \( Z \): mixture fraction
- \( <Z>\): Favre-averaged mixture fraction

**Greek letters**
- \( \delta_L \): laminar flame thickness (m)
- \( \varepsilon \): turbulent dissipation rate (m²/s³)
- \( k \): turbulent kinetic energy (m²/s²)
- \( \rho \): kinematic viscosity (m²/s)
- \( \tau_{flow} \): characteristic flow time (s)
- \( \tau_{chem} \): characteristic chemical time (s)
- \( \phi_i \): local equivalence ratio
- \( \phi_j \): equivalence ratio in the premixed jet

**Abbreviations**
- NBB: no-bluff-body
- RZ: recirculation zone
- WBB: with-bluff-body

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range of fuels. Szegő et al. [8,9] experimentally investigated the effect of fuel dilution (diluting type and dilution level), heat extraction, air preheating and global equivalent ratio on the reaction zone characteristics and NOx emissions on a parallel multi-jet MILD combustion burner system. They found that air preheating is not necessary to realize MILD combustion while heat extraction and fuel dilution is beneficial for the establishment of MILD combustion. NOx emissions are less than 60 ppm and decreases with increasing heat extraction and fuel dilution level. Mi et al. [10] experimentally and numerically studied the performance of MILD combustion in a lab-scale furnace, varying the air-fuel momentum rate and air-fuel premixing. They concluded that there exits a critical momentum rate of the inlet reactants, below which MILD combustion cannot be realized. Mi et al. [11,12] also numerically investigated the effect of air and fuel nozzle diameter, air preheat temperature, fuel dilution, injection angle and injection separation of air and fuel on the establishment of non-premixed MILD combustion. They found that all parameters will influence the combustion characteristics through two crucial flow quantities, the recirculation ratio and the fuel-jet penetration distance. Li et al. [13] investigated the effect of fuel-air mixing pattern on the establishment of MILD combustion and reported that it is easy to realize MILD combustion in fully premixed condition but difficult in partially premixed condition. Recently, Kruse et al. [14] found that a high pressure increases NOx emissions and hinders the establishment of MILD combustion in gas turbine.

Turbulent jet flame is a good experimental configuration for fundamental studies [15–21]. Dally et al. [15] studied the reaction characteristics of a turbulent CH4/H2 jet flame in hot coflow (JHC) and found that MILD combustion can be realized under low oxygen level. Cabra et al. [16,17] examined the lift-off behavior in a non-premixed H2/N2 and a premixed CH4/air jet flame and revealed that the coflow temperature has a great impact on the flame lift-off height. Gkagkas et al. [18] investigated the combustion characteristics of the CH4/air jet flame and found that the flame stabilization is dominant by auto-ignition and the lift-off height has a significant sensitivity to the coflow composition. Wang et al. [19] numerically investigated the effect of coflow oxygen level (XO2, c) and temperature (Tc) on the realization of MILD combustion and finally proposed a useable classification of combustion regimes by XO2, c and Tc. Mei et al. [20] and Dai et al. [21] studied the combustion characteristics of a methane jet flame in an O2/CO2 (and O2/H2O) coflow and reported that the oxy-fuel (and oxy-steam) reaction zone is larger than that in air-fuel combustion. Therefore, MILD combustion is expected to occur more easily for the JHC flame diluted by CO2 or H2O rather than by N2.

Previous studies, e.g., Refs. [4–21], focused on the comparison of flameless MILD combustion and flame-visible combustion through varying inlet and boundary conditions, i.e., nozzle arrangement (e.g., ejection angle), inlet temperature and velocity, fuel type, fuel/oxygen diluting type and dilution level, furnace pressure and heat extraction degree. Those works were all on the establishment conditions and reaction characteristics of MILD and flame-visible combustion without using any flame stabilizers. On the other hand, designers of industrial burners and gas turbine combustors commonly use a bluff-body or multiple bluff-bodies to achieve stable traditional flames [22–25]. However, the MILD combustion has never been differentiated from a truly conventional flame. This stimulates the present work to characterize MILD combustion versus typical traditional combustion for applications. Additionally, previous works were mainly on non-premixed MILD combustion, while little work has been done on premixed MILD combustion [17,18], which is also very important in fundamental research and applications. So, a detailed comparison between premixed MILD combustion and traditional bluff-body combustion in methane jet flame is to be conducted in this work. More specifically, the present study uses identical inlet and outer boundary conditions for both cases of investigation but sets a conical bluff body near the jet nozzle exit to alter the inner flow structure for the traditional flame.

With the bluff body, the reactants are objected by the bluff body...
and a stabilized flame is formed behind it [23–25]. Removing the bluff body, the premixed jet may be ignited far downstream by the hot coflow, and so MILD combustion may be established due to strong jet entrainment of vitiated coflow [15–17]. The aim of this work is to deeply investigate the differences between such MILD combustion and traditional bluff-body stabilized combustion. More specifically, the present study is to differentiate these two cases of combustion by distinguishing their flow fields, reaction zone characteristics and NOx formations and thus emissions. The main objectives are:

1. To detail the establishment processes of the MILD combustion and traditional bluff-body stabilized combustion;
2. To understand the distinct reaction-zone characteristics and flame modes of the two combustion processes;
3. To quantify the NOx formation and emissions routes from the two combustion processes.

2. Computational details

2.1. Numerical setup

The present calculations are based on the experimental configuration of the vitiated coflow burner (VCB) of Cabra et al. [17], as briefly described here. The VCB consists of a central jet nozzle (inner diameter \(d = 4.57 \text{ mm}\)) and a surrounding perforated plate with diameter of 210 mm. The central jet is a mixture of methane and air, with equivalent ratio \(\Phi_j = 4.4\) and temperature \(T_j = 320 \text{ K}\). The surrounding plate was drilled with 2200 holes (1.58-mm diameter), on which premixed lean H\(_2\)/air flames were stabilized; their combustion products formed the vitiated coflow with bulk velocity \(U_C = 5.4 \text{ m/s}\) and temperature \(T_C = 1350 \text{ K}\). The central jet nozzle extends 70 mm downstream of the perforated plate surface to ensure uniform coflow properties. The jet exit velocity \(U_j\) is 100 m/s, corresponding to the Reynolds number of \(Re = 28000\). The other inlet conditions in the premixed jet and coflow are summarized in Table 1. Moreover, Cabra et al. [17] measured single-point temperatures and species mass fractions using the Raman-Rayleigh-LIF technique. Favre-averaged temperature and mass fractions of CH\(_4\), H\(_2\), O\(_2\), H\(_2\)O, OH, CO and CO\(_2\) and their fluctuations were computed. In addition, visible chemiluminescence was used to determine the flame front position and lift-off height.

For the present study, to compare MILD combustion and traditional bluff-body stabilized combustion, a hollow conical bluff body is placed at \(x = 1.0d\) to form a conventional flame behind it, see Fig. 1. The jet exit velocity and coflow velocity are reduced to 50 m/s and 1 m/s, respectively, to stabilize the traditional flame in the recirculation zone. The coflow oxygen level of 6% (in volume) is taken to establish MILD combustion with no bluff-body. Three jet equivalent ratios \((\Phi_j = 0.8, 1.0\) and 1.2) are chosen to study the fuel-lean, stoichiometric and fuel-rich flames. The mole fraction of CH\(_4\)

Table 1

<table>
<thead>
<tr>
<th>Cases</th>
<th>Central jet (U_j) (m/s)</th>
<th>(T_j) (K)</th>
<th>(X_{CH_4})</th>
<th>(X_{O_2})</th>
<th>(X_{N_2})</th>
<th>(\Phi_j)</th>
<th>Hot coflow (U_c) (m/s)</th>
<th>(T_c) (K)</th>
<th>(X_{O_2})</th>
<th>(X_{N_2})</th>
<th>(X_{H_2O})</th>
</tr>
</thead>
<tbody>
<tr>
<td>1 EXP</td>
<td>100</td>
<td>320</td>
<td>0.330</td>
<td>0.150</td>
<td>0.520</td>
<td>4.4</td>
<td>5.4</td>
<td>1350</td>
<td>0.12</td>
<td>0.15</td>
<td>0.73</td>
</tr>
<tr>
<td>2 NBB0.8(^a)</td>
<td>50</td>
<td>320</td>
<td>0.167</td>
<td>0.417</td>
<td>0.416</td>
<td>0.8</td>
<td>1.0</td>
<td>1250</td>
<td>0.06</td>
<td>0.94</td>
<td>0.00</td>
</tr>
<tr>
<td>3 NBB1.0</td>
<td>50</td>
<td>320</td>
<td>0.167</td>
<td>0.333</td>
<td>0.500</td>
<td>1.0</td>
<td>1.0</td>
<td>1250</td>
<td>0.06</td>
<td>0.94</td>
<td>0.00</td>
</tr>
<tr>
<td>4 NBB1.2</td>
<td>50</td>
<td>320</td>
<td>0.167</td>
<td>0.278</td>
<td>0.555</td>
<td>1.2</td>
<td>1.0</td>
<td>1250</td>
<td>0.06</td>
<td>0.94</td>
<td>0.00</td>
</tr>
<tr>
<td>5 WBB0.8</td>
<td>50</td>
<td>320</td>
<td>0.167</td>
<td>0.417</td>
<td>0.416</td>
<td>0.8</td>
<td>1.0</td>
<td>1250</td>
<td>0.06</td>
<td>0.94</td>
<td>0.00</td>
</tr>
<tr>
<td>6 WBB1.0</td>
<td>50</td>
<td>320</td>
<td>0.167</td>
<td>0.333</td>
<td>0.500</td>
<td>1.0</td>
<td>1.0</td>
<td>1250</td>
<td>0.06</td>
<td>0.94</td>
<td>0.00</td>
</tr>
<tr>
<td>7 WBB1.2</td>
<td>50</td>
<td>320</td>
<td>0.167</td>
<td>0.278</td>
<td>0.555</td>
<td>1.2</td>
<td>1.0</td>
<td>1250</td>
<td>0.06</td>
<td>0.94</td>
<td>0.00</td>
</tr>
</tbody>
</table>

\(^a\) NBB0.8 denotes no-bluff-body and \(\Phi_j = 0.8\).

Fig. 1. Schematic diagram and orthogonal structured grid of the computational domain for the no-bluff-body (NBB) cases (a1, a2) and with-bluff-body (WBB) cases (b1, b2).
(XCH4) is kept constant for different \( \phi \) to keep the same power rate (\( P = 4.9 \) kW). The detailed inlet conditions are also summarized in Table 1.

Considering the symmetry of the VBC configuration, a simplified two-dimensional (2-D) computational model is used to reduce computational cost. As shown in Fig. 1, the computational domain spans 1000 mm (about 219d) axially and 200 mm (about 44d) radially. The stretched structured grids with 14,600 cells and 20,000 cells are adopted for the cases of no-bluff-body (NBB) and with-bluff-body (WBB) after the verification of grid independency with a coarser grid of 6700 cells and a fine grid of 24,500 cells (see section 3.1). The smallest and largest grid sizes are 0.03d and 2.2d, respectively.

### 2.2. Computational methods

The commercial software ANSYS Fluent 17.2 is currently used to solve the related transport equations, i.e., those of the mean mass conservation, axial and radial momentums, turbulent kinetic energy and its dissipation rate, Favre-averaged mass fractions for each species, radiation intensity and energy conservation. According to the previous studies [26,27], a modifies \( k-c \) model, i.e., adjusting \( C_{\mu} \) from 1.44 to 1.6, with the standard wall function, is adopted to emulate the turbulent flows. A Lagrangian particle-based Monte-Carlo method is used to solve the probability density function (PDF) transport equations of temperature and chemical compositions. The mixing model for the PDF equations is modified Curl (M-Curl) model, with modification of mixing constant to 2.3 according to the suggestion of Gkagkas et al. [18]. The particle number in each grid cell is 20. The detailed mechanism of GRI-Mech 2.11 [28], with 49 species, radiation intensity and energy conservation. According to the previous studies [26,27], a modifies \( k-c \) model, i.e., adjusting \( C_{\mu} \) from 1.44 to 1.6, with the standard wall function, is adopted to emulate the turbulent flows. A Lagrangian particle-based Monte-Carlo method is used to solve the probability density function (PDF) transport equations of temperature and chemical compositions. The mixing model for the PDF equations is modified Curl (M-Curl) model, with modification of mixing constant to 2.3 according to the suggestion of Gkagkas et al. [18]. The particle number in each grid cell is 20. The detailed mechanism of GRI-Mech 2.11 [28], with 49 species and 279 reactions, is applied to simulate chemical reactions. Combining the transported PDF model and detailed mechanism is a good choice for modeling both MILD combustion [29] and traditional combustion [23]. To accelerate the computational process, we use the in situ adaptive tabulation (ISAT) model developed by Pope [30]. The ISAT tolerance is set to be 5 \( \times \) 10^{-5} according to Masri et al. [31]. The discrete ordinate (DO) model [32] together with the weighted sum of gray gas model (WSGGM) is employed as the radiation model. The SIMPLE scheme is adopted for solving the pressure-velocity coupling. The second order upwind scheme is applied for spatial discretization to improve the accuracy of calculations. The convergence criteria are: (1) the residuals for energy and radiation equations are less than 10^{-5} and (2) the residuals for other equations are less than 10^{-5} and (2) the variations of the area-weighted outlet velocity and Favre-averaged temperature are less than 0.1 m/s and 1.0 K, respectively.

### 3. Model validation

#### 3.1. Check to grid independency

To check the present mesh suitability, three orthogonal structured grids are used to model the experimental case (EXP). The cell number for the coarse, moderate and fine meshes are 6,700, 14,600 and 24,500, respectively. To quantify the mixed degree between the central premixed jet and the hot vitiated coflow, we adopt the mixture fraction (\( Z \)) defined by Bilger et al. [33] viz.

\[
Z = \frac{2 \left( Y_c - Y_{cc} \right)}{W_c} + \frac{1}{2} \left( \frac{Y_{j,c} - Y_{j,cc}}{W_c} - \frac{Y_{j,c} - Y_{j,cc}}{W_o} \right)
\]

where \( Y_i \) and \( W_i \) are the mass fraction and atomic mass of \( i \)th elements (C, H and O); \( Y_{j,c} \) and \( Y_{j,cc} \) are the mass fractions of \( j \)th elements in the central jet and in the vitiated coflow, respectively.

**Fig. 2.** Comparison of axial velocity (\( U_x \)), Favre-averaged mixture fraction (\( <Z> \)), Favre-averaged temperature (\( <T> \)) and its root-mean-square (RMS) value (\( \langle \bar{T} \rangle \)), Favre-averaged species mass fractions (include main component \( <Y_{OH}> \) and minor component \( <Y_{OH}> \)) on the centerline for the three grids. High consistency of the profiles of \( U_x \) and \( <Z> \) among these grids is evident. However, for the coarse mesh, the profiles of temperature and species concentrations are different with the other two grids. And the sharp decline of peak \( <T> \) and \( \langle \bar{T} \rangle \) for the coarse mesh are about 10d downstream of those for the other two grids. And the sharp decline position of \( <Y_{OH}> \) is also delayed. Therefore, the reactions rates are underestimated and the ignition position is overestimated by the coarse mesh. Conversely, the results calculated with the moderate mesh are in line with those of the fine mesh. Therefore, the grid with 14,600 cells is adequate to model such a premixed jet flame in the vitiated coflow.

**Fig. 3.** Displays the center-plane contours of Favre-average temperature (\( <T> \)) and mass fraction of OH (\( <Y_{OH} \)) for the coarse, moderate and fine meshes. Evidently, the flame front occurs at \( x = 35d \) for the moderate and fine meshes while it appears at \( x = 42d \) for the coarse mesh. Moreover, the high temperature region (\( >2100K \)) and strong-reaction region (\( <Y_{OH} > \) over 0.002) of
the coarse mesh are smaller than those calculated with the moderate and fine meshes. The maximum Favre-averaged temperature $<T>_{\text{max}}$ and maximum Favre-averaged OH mass fraction $<Y_{\text{OH}}>_{\text{max}}$ are also underestimated by the coarse mesh. Therefore, the grid with 6700 cells is too coarse that it is not applicable for the calculation. Relatively, the results calculated with moderate grid are highly close to those of the fine mesh, with the differences in $<T>_{\text{max}}$ and $<Y_{\text{OH}}>_{\text{max}}$ less than 2K and $10^{-3}$, respectively. So, the moderate grid with 14,600 cells is chosen for those calculations whose results are presented below.

3.2. Experimental validation

Present simulations, with the transported PDF model and fully detailed chemistry mechanism of GRI-Mech 2.11, are validated by the premixed CH$_4$/air jet flame experiment of Cabra et al. [17]. The measured and calculated Favre averaged mixture fraction ($<Z>$), temperature ($<T>$) and mass fractions of major and minor species ($<Y_{\text{CO2}}>$, $<Y_{\text{CO}}>$ and $<Y_{\text{H2}}>$) are demonstrated in Fig. 4. Overall, the numerical results of $<Z>$, $<T>$, $<Y_{\text{CO2}}>$ and $<Y_{\text{CO}}>$ are in accordance with the experimental data. The predictions of $<Y_{\text{H2}}>$ and $<Y_{\text{H2O}}>$ agree well with the measurements at $x < 60d$. At $x > 60d$, the modeling slightly overvalues $<Y_{\text{CO2}}>$ and $<Y_{\text{H2O}}>$, Cabra et al. [17] pointed out that this should be attributed to the little penetration of ambient air into the measurement region in the experiment.

Fig. 5 presents the radial distributions of the Favre-averaged mixture fraction ($<Z>$), Favre-averaged temperature ($<T>$) and its RMS value ($\sigma$). As clearly shown, the agreement between the modeled and measured profiles of $<Z>$, $<T>$ and $\sigma$ is reasonably good, allowing some quantitative discrepancies for the temperature fluctuation $\sigma$ in the downstream region. Therefore, the ignition process of the premixed methane/air jet flame can be well captured by the present numerical model.

Above all, the current modeling settings have been validated to enable appropriate CFD simulations for the present study that predict the premixed flame characteristics.

4. Combustion establishment process

4.1. Global analysis on contour charts

Fig. 6 presents the center-plane contours of axial velocity ($U_x$) and Favre-averaged mixture fraction ($<Z>$) and temperature ($<T>$) for the no-bluff-body (NBB) and with-bluff-body (WBB) cases with jet equivalent ratio of $\Phi_j = 1.0$. For the NBB case, $U_x$ and $<Z>$ maintain high values (almost as high as those at the jet exit), see Fig. 6-a1 and 6-a2, for a considerably long distance (about 12$d$) as the premixed jet issues into the coflow. This region is so-called the jet “potential core” region. Combustion cannot be established here because of the extremely high local velocity (see Fig. 6-a3). Farther downstream, the central jet entrains a large amount of hot coflow, so that both $U_x$ and $<Z>$ decrease gradually with $x$. Within the entrainment process, the premixed reactants are simultaneously diluted and heated by the co-flowing low-oxygen mixture. The auto-ignition occurs once the reactant temperature has been elevated above the auto-ignition temperature ($T_{\text{ui}} = 813$ K), finally forming a stable lifted flame quite far away downstream from the nozzle exit (see Fig. 6-a4).

Alternatively, when a conical bluff body is placed downstream and near the jet exit, the premixed jet will be hindered and have to flow around the bluff body (see Fig. 6-b1). As a result, a recirculation zone (RZ) will form behind the bluff body, where a backflow

![Fig. 3. Center-plane contours of Favre-average temperature ($<T>$) and mass fraction of OH ($<Y_{\text{OH}}>$) for the coarse, moderate and fine meshes.](image)

![Fig. 4. Favre-averaged mixture fraction ($<Z>$), temperature ($<T>$) and mass fractions ($<Y_{\text{CO2}}>$, $<Y_{\text{CO}}>$ and $<Y_{\text{H2}}>$) on the centerline. Solid lines represent numerical results (CFD). Hollow squares and triangles are experimental measurements (EXP).](image)
occurs. Correspondingly, most of the premixed reactants will be trapped and thus stay in the RZ for a sufficiently long period of time, which may be treated approximately as the residence time \([22]\). In such conditions, high temperature patching (replicating the spark ignition in experiments) is used to ignite the reactants in the RZ and thus to develop a flame there. This flame then continuously ignites the incoming reactants and acts as a stable flame of the expanded recirculation zone (see Fig. 6-b3 and 6-b4).

For the NBB case, the central jet is slowly heated by the hot coflow (1250 K) when flowing downstream and finally the ‘flame’ is stabilized at about \(x = 50d\). At that position, the premixed reactants have been fully diluted by the low-oxygen coflow (6% in volume). The maximum temperature is about 1600 K, corresponding to a temperature rise of about 350 K, thus it falls in the mode of MILD combustion. In contrast, for the WBB case, the mixing process is greatly intensified by the bluff body (see Fig. 6-b2). The premixed jet is simultaneously diluted by the high temperature combustion products in the RZ and by the hot coflow outside, so the mixture fraction decreases quickly and temperature rises promptly. Thus, the reactants are immediately burnt in the RZ and then flame stabilizes and heat rapidly releases there. The maximum temperature is over 2580K and the combustion is a typical conventional flame.

To conclude, the ignition processes are totally different for the NBB and WBB cases. For the NBB case, the premixed reactants are heated and diluted by the hot vitiated coflow, then auto-ignition occurs and stable lifted MILD combustion “flame” is formed. However, for the WBB case, the incoming premixed reactants are continuously ignited by the high temperature combustion products in the RZ, so a conventional flame is stabilized behind the bluff body. Next, we will further discuss the ignition processes of these two regimes using the scatterplots at different axial locations.

4.2. Scatterplot analysis

To compare the two combustion processes insightfully, the scattered data of temperature \((T)\) and mass fraction of OH \((Y_{OH})\) against the mixture fraction \((Z)\) and the local equivalence ratio \((\phi)\) are plotted in Figs. 7 and 8. (To inspect very small \(Y_{OH}\) properly, logarithm is used for \(Y_{OH}\) in Fig. 8. Both \(Z\) and \(\phi\) are 1.0 in the premixed jet and 0.0 in the vitiated coflow. So, they both range from...
0.0 to 1.0.) Such scatterplots represent the joint distributions of $T$ and $Y_{\text{OH}}$ with $Z$ and $\Phi$ that help us to understand the scalar structure of the flame. Of note, we select data from 100 iteration steps, with the step interval of 10 iterations, to draw the scatterplots; and each data ensemble is produced by combining the whole radial profile at each axial location. For reference, the curves of the pure mixing and equilibrium temperature and $Y_{\text{OH}}$ from perfectly stirred reactor (PSR) calculations are also plotted. Pure mixing means mere mixing of the premixed jet with hot coflow without any reaction while equilibrium represents fully chemical reactions.

For the NBB case, all temperature points fall on the purely mixing line with $Y_{\text{OH}} = 0$ at $x < 30d$, which means that no reactions occur in the region upstream of $x = 30d$. At $x = 40d$, tiny OH appears at $\Phi < 0.4$ (see Fig. 8), indicating the occurrence of auto-ignition from here. From $x = 50d$ to $70d$, the temperature and OH points fall on the equilibrium line at low $Z$ or $\Phi$ values, and this portion widens as $x$ increases. However, near the high end of $Z$ or $\Phi$, the points fall between the pure mixing and equilibrium line. Farther downstream at $x = 100d$, almost all temperature and OH samples reach the equilibrium line, reflecting the fully chemical reactions and heat release there. The combustion event occurs in a long region from about $40d$ to $<150d$. During this process, auto-ignition firstly occurs at lower $Z$ or $\Phi$ (mixing layer) for higher initial temperatures and shorter ignition delay there, then the ‘flame front’ propagates toward higher $Z$ or $\Phi$ (central jet, Fig. 6-a4), agreeing well with the results of Cabra et al. [16,17]. Farther downstream at $x = 150d$ (see Fig. 8), chemical reactions become weak with reactants burning out, so all the OH points drop off the equilibrium line. It is interesting to see that all the temperature points still lie along the equilibrium line perhaps because of a very low rate of heat transfer from the reaction region to the hot coflow. At the end of the computational domain ($x = 218d$), low OH concentration exists at $Y_{\text{OH}} < 10^{-4}$ (see Fig. 8), indicating some very weak combustion is still going on.

For the WBB case, distributions of scatter points are totally different in the near field because the bluff body considerably enhances the turbulent mixing and accelerates chemical reactions through a recirculating zone (RZ) behind it. At $x = 0.8d$, all temperature and OH points at $0 < Z$, $\Phi < 1$ fall on the pure mixing line, indicating no reaction and heat release here. At $x = 1.6d$, i.e., the end of the bluff body, the premixed reactants mix with both the extremely hot combustion products in the recirculation zone with $Z = 0.8$ and the vitiated coflow outside with $Z = 0$ (see Fig. 6-b2). That is, there are two mixing layers. If follows that the temperature and OH samples split into two branches. The lower-temperature branch occurs over a wide range of $Z$ from 0.0 to about 1.0 and follows the line of pure mixing, representing the nonreactive mixing between the premixed jet and the vitiated coflow. The maximum $Z$ is about 1.0 because there are still some premixed reactants that are almost totally undiluted (see Fig. 6-b2). The other branch occurs at $0.8 < Z < 1$ and belongs to the mixing process between the premixed jet and the central RZ combustion products of extremely high temperature (>2500 K, see Fig. 6-b2). Chemical reactions in the RZ take place so rapidly that the temperature and $Y_{\text{OH}}$ scatter points for the combustion products distribute on both lean and rich-fuel equilibrium lines, ranging the temperature (and $Y_{\text{OH}}$) between 320 K and about 2600 K (0 and about 0.013). Downstream to $x = 2.4d$, the premixed reactants are diluted and thus the maximum $Z$ decreases to about 0.92. Within the dilution process, more premixed reactants are heated and also ignited rapidly by the RZ combustion products ($T > 2500$ K). Consequently, new reactions begin at $Z > 0.7$ so that many samples for temperature and OH move away from the purely mixing line. Worth noting is that some scatter points are still kept on the equilibrium lines at $0.76 < Z < 0.88$. The recirculation carries low-$Z$ gases upstream and thus extends $Z$ to 0.76. The RZ flame propagates across the mixing layer between the combustion products and the premixed reactants, thus extending $Z$ to 0.88. Farther downstream at $x = 4.8d$, the premixed jet is well diluted and the two mixing layers join up. All temperature and OH points except their peak values are between the mixing line and the equilibrium line. As $x$ increases to 6.4d, they move closer to the lean-fuel equilibrium line. At $x = 10d$, all the reactive gases across the jet are fully mixed, so that all temperature and OH points fall on the chemical equilibrium line. Farther downstream, all the reactants are burning out. At $x = 70d$ (see Fig. 8), chemical reactions weaken dramatically and OH points drop off the equilibrium line. Similar to the NBB case, all the temperature points still lie along the equilibrium line because heat transfers at a very low rate from the central region to the hot coflow. At $x = 218d$ (computational domain end, Fig. 8), $Y_{\text{OH}}$ becomes nearly zero, indicating the end of chemical reactions.

5. Reaction zone characteristics

5.1. Reaction zone

Following the work of Mei et al. [20,27], we consider the contour of $R_{\text{CO}} = 0.05$ as the boundary of the reaction zone, where $R_{\text{CO}}$ is defined by

$$R_{\text{CO}} = \frac{<Y_{\text{CO}}>}{<Y_{\text{CO}}>_{\text{max}}}$$

(2)

where $<Y_{\text{CO}}>_{\text{max}}$ is the maximum Favre-averaged CO mass fraction in the whole computational domain. Fig. 9 demonstrates the contour distributions of Favre-averaged CO mass fraction ($<Y_{\text{CO}}>$) for the no-bluff-body (NBB: $\Phi_i = 0.8$, 1.0 and 1.2) and with-bluff-body (WBB: $\Phi_i = 0.8$, 1.0 and 1.2) cases. Several observations can be made from the plots. Firstly, for the NBB case, the CO levels are less than those of WBB case by one to two orders of magnitude, indicating that reactions occur much more rapidly in the WBB case.
Secondly, \(<\text{CO}>_{\text{max}}\) decreases with increasing \(\Phi_j\) for the NBB case, but the trend is totally reversed for the WBB case. This is due to different reaction patterns for the WBB and NBB cases. For the WBB case, the \(<\text{CO}>\) peak appears in the recirculation zone and only the incoming premixed reactants can affect the reactions there (the vitiated coflow has no impact). As \(\Phi_j\) increases, the oxygen in the jet becomes deficient or the jet becomes lean-fuel, so CO will accumulate behind the bluff body and \(<\text{CO}>_{\text{max}}\) arises. However, for the NBB case, the premixed reactants are mixed and diluted by the low-oxygen coflow as \(x\) increases, so the deficient oxygen is replenished. Moreover, as \(\Phi_j\) increases, the complete combustion of the premixed reactants requires the NBB jet to entrain more oxygen from the coflow over a longer distance, hence resulting in more dilution. Therefore, in the NBB case, the increase of \(\Phi_j\) slows combustion reactions and so decreases \(<\text{CO}>_{\text{max}}\).

Thirdly, the reaction zone (bounded by the black line) is much larger for the NBB case comparing to the WBB case. The lower temperature and slower reactions caused by the strong dilution of the low-oxygen coflow mean that the reactants need more time and space to burn out. Therefore, the reaction zone is significantly enlarged for the NBB case.

5.2. Burning mode

To further analyze the burning mode in the reaction zone, we use the flame index (\(FI\)) defined by Yamashita et al. \[34\] as

\[
FI = \frac{\nabla(Y_F) \cdot \nabla(Y_O)}{||\nabla(Y_F)|| ||\nabla(Y_O)||}
\] (3)

where \(\nabla(Y_F)\) and \(\nabla(Y_O)\) are the gradients of the Favre-averaged mass fractions of fuel (\(<\text{CH}_4>\)) and oxygen (\(<\text{O}_2>\)), respectively. The value of \(FI\) is between \(-1\) and \(1\), where \(FI = 1\) represents a fully premixed flame and \(FI = -1\) stands for a fully non-premixed flame. Therefore, we assume that when \(FI \geq 0.5\), the flame is a well-premixed flame; when \(FI\) is between \(-0.5\) and \(0.5\), it is a partially premixed flame; when \(FI \leq -0.5\), it is a non-premixed flame. Note that originally \(FI\) is not related to combustion reactions. Only if there is a flame, \(FI\) can be used to decide what kind of flame it is. Hence, we will use it only in the reaction zone. It is also important to note this: for the NBB and WBB cases, although the reactants are initially fully mixed and thus issue as a premixed jet, the MILD combustion and traditional bluff-body flame cannot be treated as a
fully premixed flame. This is because the accomplished combustion processes have to be involved by the turbulent mixing between the premixed jet and hot coflow.

Fig. 10 demonstrates the contour distributions of flame index (FI) in the reaction zone for the NBB and WBB cases. The dashed black lines are the boundaries of the reaction zone at which $R_{CO} = 0.05$, while the white solid lines represent contours of $FI = 0.5$. As expected, no non-premixed flame occurs in both WBB and NBB cases where $FI$ is above $-0.5$ in the whole reaction zone. Clearly, the distributions of $FI$ show totally different characteristics for the NBB and WBB cases. For the NBB case, the premixed jet is slowly diluted by the hot coflow and so can maintain high speed and high Z when flowing downstream. The NBB turbulent mixing is not strong when comparing to the WBB case. Moreover, $\nabla (Y_f)$ and $\nabla (Y_O)$ are almost in the same direction so that $\nabla (Y_f) \cdot \nabla (Y_O)$ is high and $FI > 0.5$ for $x \leq 70d$ in the NBB case at $\Phi_f = 0.8$. Farther downstream, $FI$ decreases to less than 0.5 due to the entrainment of large amount of low-oxygen coflow and the different gradient directions of fuel and oxidant. So, the flame becomes partially premixed flame. Within the whole reaction zone, the well premixed flame accounts for a large proportion. In addition, as $\Phi_f$ increases, the well premixed ‘flame’ region shifts downstream together with the whole reaction zone.

For the WBB case, the turbulent mixing is intensified by the bluff
body, so the mixing process of the premixed jet with combustion products in the recirculation zone (RZ) and with the vitiated coflow are both greatly enhanced. So, the gradient directions of fuel and oxidant are disordered and $\Phi$ is low. Therefore, the partially premixed flame region is quite large and the well premixed flame region is confined near to the edge of the RZ. Similar to the NBB case, the increase of $\Phi$ makes both WBB flame regions to move downstream.

To quantify the combustion characteristics in the reaction zone, the reaction zone volume ($V_R$) and the ratio of the premixed reaction zone ($V_{R,P}/V_R$) are calculated and exhibited in Fig. 11(a) and (b), respectively. Evidently, the reaction zone volume for the NBB case is about 0.0015 m$^3$ for $\Phi=0.8$, which is 22 times as that for the WBB case. As $\Phi$ increases, the oxygen fraction in the premixed jet reduces, so the fuel needs to entrain more oxidant from the low-oxygen coflow to burn out and thus $V_R$ increases for both NBB and WBB cases. More specifically, the ratio of NBB volume to WBB volume reduces slightly with increasing $\Phi$.

Fig. 11b shows that the proportion of the mainly premixed part, $V_{R,P}/V_R$, is about 0.4 for the NBB case at $\Phi=0.8$, which is more than twice of that for the WBB case (about 0.15). This difference can be explained. In the WBB case, the turbulent mixing is strengthened by the bluff body and the directions of $\nabla(V_R)$ and $\nabla(V_O)$ are disordered. Therefore, $\nabla(V_R)$, $\nabla(V_O)$ is low and the mainly premixed part is quite small relative to the whole reaction zone (see Fig. 10). As $\Phi$ increases, the ratio $V_{R,P}/V_R$ decreases significantly for the NBB case and increases slightly for the WBB case. This can be attributed to different conditions of flow, mixing and reactions for the two cases. For the NBB case, the reaction zone becomes larger with increasing $\Phi$, but the mainly premixed part remains nearly unchanged for the similar entraining and mixing conditions, so the premixed proportion decreases. However, the situation changes for the WBB case: as $\Phi$ increases, the overall oxidation weakens and the temperature reduces (see Fig. 14a). Thus, both turbulent mixing processes of the premixed reactants with the RZ combustion products and with hot coflow become weakened. So, for the WBB case, the increase of $\Phi$ enlarges the premixed part (see Fig. 10). At the same time, the reaction zone ($V_R$) also increases with increasing $\Phi$. Therefore, the proportion of the mainly premixed part remains almost constant at different $\Phi$ for the WBB case.

5.3. Flame classification

To compare the NBB and WBB flame modes in a more fundamental way, we calculate the turbulent Reynolds number ($Re_t$) and the Damkohler number ($Da$) to draw the Borghi diagram [35] for the flame classification. The turbulent Reynolds number is defined as

$$Re_t = \frac{u' l_0}{\nu}$$

where $u'$ is the root-mean-squared fluctuation velocity, $l_0$ is the integral length scale and $\nu$ is the kinematic viscosity. Damkohler number ($Da$) is defined as the ratio of a characteristic flow time ($\tau_{\text{flow}}$) to a characteristic chemical time ($\tau_{\text{chem}}$), viz.,

$$Da = \frac{\tau_{\text{flow}}}{\tau_{\text{chem}}} = \frac{l_0}{\delta_1 S_L}$$

where $\delta_1$ and $S_L$ are the laminar flame thickness and the laminar

![Fig. 11](image1.png)

**Fig. 11.** (a) Reaction zone volume ($V_R$) for the NBB and WBB cases and ratio of NBB volume to WBB volume and (b) the proportion of mainly premixed reaction zone ($V_{R,P}/V_R$) for different cases.

![Fig. 12](image2.png)

**Fig. 12.** (a) Laminar flame speed ($S_L$) against the local axial velocity ($U_x$) and (b) Damköhler number ($Da$) versus the turbulent Reynolds number ($Re_t$).
flame speed, respectively. Since we use the modified $k$-$\varepsilon$ model as the turbulent model, $u'$ and $l_0$ can be calculation by

$$u' = \left( \frac{2k}{3} \right)^{1/2}, \quad l_0 = C_d k^{3/2} / \varepsilon$$

and $\delta_L$ can be estimated by

$$\delta_L = 2\alpha / S_L$$

where $k$ is the turbulent kinetic energy, $\varepsilon$ is the turbulent dissipation rate, $C_d$ is the constant of 0.09, and $\alpha$ is the thermal diffusion coefficient. All quantities can be obtained using the calculation results.

The remaining parameter for the flame classification is the laminar flame speed ($S_L$) which can be calculated using CHEMKIN-PRO [36]. We choose five representative positions (i.e., red dots in Fig. 8) in the reaction zone of each case for the flame classification. Fig. 12 displays the scatterplots of the laminar flame speed ($S_L$) against the local axial velocity ($U_x$) and Damköhler number ($Da$) against the turbulent Reynolds number ($Re_t$). For the NBB case, see Fig. 13a, the laminar flame speed (~0.1 m/s) is evidently lower than the local flow speed, so the flame cannot be stabilized through flame propagation. For such a case, auto-ignition is the only way to establish and stabilize the ‘flame’, which is the MILD combustion, consistent with the previous work [18,37]. For the WBB case, among the selected five locations, there are two at $U_x < 0$, one where $S_L = U_x$, and two where $S_L < U_x$. Therefore, the conventional flame can be established by the ‘pilot’ flame due to the recirculation zone and by flame propagation.

For the premixed combustion, fundamentally, there are three reaction regimes: i.e., (I) reaction sheets, (II) flamelets in eddies and (III) distributed reactions. Fig. 12b illustrates these regimes by two solid lines and shows where the present cases are located. Above the red line of $l_0/D_L = 1$, chemical reactions occur in Regime (I); below the black line of $l_0/D_L = 1$, reactions occur in Regime (III). Between the two solid lines, combustion takes place in Regime (II), where the flame is broken into small pieces by large-scale eddies. Obviously, all the data points for the WBB case are located in Regime (I) with relatively high $Da$ and strong turbulence. So chemical reactions are very fast and the flame thickness is quite small, smaller than the Kolmogorov scale. It follows that the WBB flame cannot be broken by any large or small eddies and maintains as continuous flame sheets. These flame sheets bend and twist

\begin{figure}[h]
\centering
\includegraphics[width=\textwidth]{fig13}
\caption{Center-plane contours of Favre-averaged mass fraction of NOx ($<Y_{NOx}>$) for the NBB and WBB cases. The black solid lines represent the boundary of the reaction zone. The maximum Favre-averaged mass fraction of NOx ($<Y_{NOx,max}$) is also shown in the contours.}
\end{figure}

\begin{figure}[h]
\centering
\includegraphics[width=\textwidth]{fig14}
\caption{The maximum Favre-averaged temperature $<T>_{max}$ (a) and the NOx emission index $EINO$ (b) against the jet equivalent ratio ($\Phi_j$) for the NBB and WBB cases.}
\end{figure}
under the effect of large eddies and finally forming a wrinkle flame, which is well visible. Conversely, all the data points for the NBB case fall in Regime (II). Their turbulent Reynolds numbers are almost the same as for the WBB case while their $Da = 10^{-2}$–$10^3$, which is much lower than that for the WBB case. Their chemical reactions take place at moderate rates and thus the flame length scale is larger than the Kolmogorov scale but smaller than the integral scale. Under such conditions, the flame will be broken up into many small pieces by large eddies. This is also confirmed by the direct numerical simulations by Minamoto et al. [38,39]. They pointed out that the sheet-like structure dominates in the conventional flame while small flame pieces are most probably observed in the MILD combustion.

### 6. Distributions and emissions of NOx

#### 6.1. Global NOx emission

Fig. 13 presents the continuous contours of Favre-averaged mass fraction of NOx ($\phi_{NOx}$), including NO and NO$_2$, for the NBB and WBB cases at $\phi_l = 0.8, 1.0$ and 1.2. For the NBB case, NOx is generated at $x > 45d$, later than the outset of the reaction zone. The temperature is low at the beginning of the reaction zone, so little NOx is produced. When the temperature rises to a higher value after $x = 45d$, NOx begins to accumulate, agreeing well with the previous work [40]. For the WBB case, NOx mainly forms in the recirculation zone and just after the stagnation point, consistent with the measurements of Dally et al. [41]. It is also evident that for the NBB case, the NOx levels are less than those of the WBB case with 2–3 orders of magnitude. This can be attributed to the lower temperature in the NBB case than in the WBB case. NOx is strongly affected by the combustion temperature (exponential relationship) and will rise quickly with temperature $> 1800K$ [42]. Moreover, as $\phi_l$ grows, $\phi_{NOx}$ decreases, especially for the WBB case. The reduction of temperature and the lowered oxygen level are the main reasons for the decreased NOx formation. For the WBB case, there is a larger temperature drop (see Fig. 14a), so $\phi_{NOx}$ goes down faster, as $\phi_l$ increases.

To quantify the NOx emissions for the NBB and WBB cases, the emission index of NOx [42] is defined as

$$EINO = \frac{m_{NOx\text{, emitted}}}{m_{\text{fuel\,burned}}} \times 1000 \text{ (g - NO/kg-CH}_4) \quad (8)$$

The mass flux of the emitted NOx is calculated at both the end of the reaction zone and the end of computational domain. The maximum Favre-average temperature ($<T_{\text{max}}>$) in the whole computational domain and the NOx emission index (EINO) versus $\phi_l$ are demonstrated in Fig. 14(a) and (b), respectively. Fig. 14a shows that $<T_{\text{max}}>$ is about 1600K for the NBB case and about 2500K for the WBB case. As a result, the NBB case can only produce the NOx emissions of $EINO < 1 \text{ (g-NO/kg-C}_4\text{H}_8)$, less than 3% of those in the WBB case. Namely, the MILD combustion (the NBB case) emits extraordinarily low NOx when comparing to the conventional combustion (the WBB case). It also evident that EINO is higher at the end of the computational domain than at the end of the reaction zone, especially at $\phi_l = 0.8$. The high temperature $N_2$ and $O_2$ in the coflow guarantee the continuous NOx formation downstream of the reaction zone. For $\phi_l = 0.8$, the reaction zone is rather small and the temperature is quite high, thus $N_2$ and $O_2$ have more time to generate more NOx in the downstream area of the reaction zone.

#### 6.2. Relative importance of various NOx formation mechanisms

Generally, there are four main formation mechanisms of NOx during the combustion of hydrocarbon fuels that contain no nitrogen [42]: i.e., thermal-NOx, prompt-NOx, N$_2$O-intermediate and NNH routes. Moreover, in fuel-rich conditions, the NOx-reburning route plays an important role in NOx destruction. To study the relative importance of the five routes, the GRI-Mech 2.11 mechanism containing detailed NOx formation and destruction mechanisms is adopted in this work, following our previous studies [43–45] (the detailed NOx reactions are not presented here). We calculate NOx from the five routes separately by performing calculations with each mechanism at a time.

Fig. 15 presents the center-plane contours of $<Y_{NOx}>$ from every route for the NBB and WBB cases with $\phi_l = 1.0$. Since NOx from the NOx-reburning route is negative and inconvenient, the absolute value is given in Fig. 16-a5 and 16-b5. Obviously, for the NBB case, the N$_2$O-intermediate route is the most significant mechanism for NOx formation, consistent with Li et al. [13,43], while the NNH route is the second important one. Guo et al. [46,47] also reported that the two crucial routes of NOx formation in the pure CH$_4$/air premixed flame are the N$_2$O-intermediate and the NNH routes. The initial reactions of NOx in N$_2$O-intermediate route for the NBB case are accelerated due to the higher concentration of H radical in the premixed flame comparing to that in the non-premixed flames. Therefore, different from the previous studies on non-premixed flames [40,44,45], the importance of NNH route is greatly intensified in the present premixed methane flames.

For the NOx formation from the thermal route, the contradictory phenomena are observed in the two cases. It is very limited in the NBB case for the low temperature (about 1600K). For the WBB case, however, NOx is mainly formed through the thermal route. The thermal route is the most sensitive mechanism to the temperature variation. The temperature in the WBB case is very high, up to 2600K, so the thermal route is immediately enhanced to the dominant mechanism. For both cases, the prompt mechanism contributes the least to the overall NOx formation, consistent with Guo et al. [46,47]. Moreover, the NOx-reburning mechanism has a great impact on the overall NOx formation in the NBB case, but its influence on the WBB flame reduces. The reason is that the NOx-reburning reactions of NOx with hydrocarbon radicals (CH$_4$) are less efficient as the temperature increasing from 1600K to 2500K [44].

To further analyze the contributions of these five NOx formation/destruction routes, we calculate the NOx mass flux ($m_{NOx}$) from every route at different axial distance ($x/d$); the results are presented in Fig. 16. For the NBB case, the significant formation of NOx appears to occur from $x = 50d$, which results predominantly from the N$_2$O-intermediate (≈50%) and NNH (45%) routes and much less from thermal and prompt routes (≈10% each). The NOx-reburning is also an important mechanism for destruction of the formed NOx (≈22%). As $x$ increases from $x = 50d$ to $x = 100d$, NOx formations and destruction from all routes increase, forming the fastest growing region of the total NOx. This region corresponds to the reaction zone. Farther downstream, the NOx production from the N$_2$O-intermediate route continues to grow significantly as $x$ increases. However, at $x = 100d$, NOx products from NNH, thermal and prompt routes remain almost constant while that from the NOx-reburning route continues to reduce. The initial reaction of N$_2$O-intermediate route N$_2$ + O = N$_2$O has a low activation energy and thus a lower temperature is favorable for this mechanism. Downstream from the reaction zone, the temperature decreases but NOx from the N$_2$O-intermediate route still increases. This can also be confirmed in Fig. 16-a2. The proportion of NOx formation from the N$_2$O-intermediate route is a little bit lower than that from...
Fig. 15. Center-plane contours of Favre-averaged mass fraction of NOx ($\langle Y_{NOx} \rangle$) from thermal (a1, b1), prompt (a2, b2), N2O-intermediate (a3, b3), NNH (a4, b4) and NO-reburning (a5, b5, absolute value) mechanisms for the NBB and WBB cases. Solid black lines represent the boundary of the reaction zone.

Fig. 16. Mass flux of NOx ($m_{NOx}$, a1, b1) and contributions of different mechanisms (a2, b2) against the axial distance ($x/d$) for the no-bluff-body (NBB: $\Phi_f = 1.0$) and with-bluff-body (WBB: $\Phi_f = 1.0$) cases.
the NNH route at $x = 50d$ and $70d$. Nonetheless, the proportion of N$_2$O-intermediate route is higher at $x > 100d$. The proportion of NO-reburning route is very significant (30%) at the beginning and reduces downstream, finally becoming constant (about 20%).

For the WBB case, the conventional flame starts to generate NOx at a very small $x$ and the NOx mass flux has a sharp rise at $x = 1.5d$. The thermal route controls the overall NOx formation, taking more than 80% contribution. The sum of contributions from other mechanisms (N$_2$O-intermediate, NNH and prompt) is less than 20%. In addition, the NO-reburning route makes a negligible contribution in the NOx emission. As $x$ increases, the NOx formation/destruction from all routes increase and thermal route keeps dominant. The fastest growing region is from 1.5$d$ to 30$d$, corresponding to the reaction zone position. At $x > 30d$, the growing speed significantly slows down. This can be explained by the reduced temperature (of about 500K) and lack of radicals like O, H and OH, which play important roles in the NOx formation [40].

For the WBB case, the thermal mechanism is always the dominant route at all values of $\phi_f$ because of high combustion temperatures. Nonetheless, the situation is different for the NBB case. Fig. 17 shows the $\phi_f$ dependences of NOx emissions (EINO, calculated at the end of the reaction zone) from different mechanisms for the NBB case. As $\phi_f$ increases, NOx emissions from the N$_2$O-intermediate and thermal routes decrease, while those from NNH and prompt routes increase. The NOx reduction from the NO-reburning route is also strengthened. This is understood when considering the variations of temperature and radicals. As $\phi_f$ increases, the temperature drops a few degrees, so the NOx production from the thermal route decreases. In addition, the O$_2$ level reduces with increasing $\phi_f$, so the concentration of O radical decreases and the concentrations of H and CH radicals increase. Therefore, the N$_2$O-intermediate route initiated by reactions of N$_2$ and O is depressed and the NNH route (and prompt route) initiated by reactions of N$_2$ and H (by reactions of N$_2$ and CH) are intensified. Moreover, the NO-reburning is also enhanced at the stoichiometric and fuel-rich conditions because of increasing CH. Finally, the overall NOx emission changes little with $\phi_f$.

7. Concluding remarks

This work has been perhaps the first study that distinguishes the MILD combustion truly with the traditional bluff-body flame when keeping the same inlet and boundary conditions. Specifically, we have characterized the MILD combustion and its NOx formation of a premixed methane jet flame in hot (1250 K) coflow against the conventional bluff-body counterpart. Detailed comparisons of their establishment processes of combustion, reaction-zone characteristics and NOx distributions are made in Sections 4-6, from which several key conclusions can be drawn below:

1. For the non-bluff-body (NBB) case, the lifted MILD combustion ‘flame’ is established in the mixing layer far downstream from the nozzle exit. Conversely, for the with-bluff-body (WBB) case, the conventional flame is formed immediately downstream from the bluff body.

2. For the NBB case, the premixed MILD combustion is basically established through auto-ignition. The premixed jet is heated and diluted by the hot vitiated coflow at 1250 K, which is substantially higher than 813 K (auto-ignition temperature), and then ignition occurs spontaneously. Finally, a lifted MILD combustion ‘flame’ is stabilized at $x > 50d$. However, for the WBB case, the oncoming premixed reactants are continuously ignited by extremely hot combustion products (>2000 K) in the recirculating zone behind the bluff body, thus forming a traditional stable flame.

3. Relative to the traditional flame, MILD combustion reactions take place at much lower rates over a far larger reaction zone. The well premixed flame accounts for a large proportion in the MILD combustion and for a small portion in the traditional flame. In the latter, the partially premixed flame is dominant. As the jet equivalent ratio ($\phi_f$) increases, the reaction zone is enlarged for both combustion modes.

4. The laminar flame speed ($S_f$) is comparable with the local axial velocity ($U_x$) in the traditional flame while $S_f < U_x$ in the MILD combustion. Importantly, the MILD combustion is composed of many mini flamelets diffusing in large-scale eddies, with relatively small values of Damkohler number, i.e. $Da = 10^{-2} - 10^0$. However, the traditional flame has much higher values of $Da (= 10^1 - 10^5)$ and correspondingly falls into the regime of reaction sheets.

5. The MILD combustion produces extremely low NOx emission, less than 3% of that from the traditional flame. In the MILD combustion, the main NOx formation mechanisms are N$_2$O-intermediate and NNH routes while the NOx-reburning route is important for the destruction of NOx. As $\phi_f$ increases from 0.8 to 1.2, the contribution of N$_2$O-intermediate route reduces while those of NNH and prompt routes grow. The NOx-reburning destruction is intensified at the fuel-rich ($\phi_f > 1$) condition. In contrast, for the conventional flame, more than 80% of NOx emissions results from the thermal route at any $\phi_f$.

At last, we would also like to remark here on some practical issues of MILD combustion based on the present work. The MILD combustion occurs and sustains due to auto-ignition, which can be characterized particularly by high flow speed, weak reactions, low $Da$, uniform temperature and composition fields, and extremely low NOx emissions. Accordingly, it differs greatly from the traditional bluff-body flame and should have advantages in numerous applications.

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**Fig. 17.** (a) NOx emission index (EINO) and (b) contributions of different mechanisms against the jet equivalence ratio ($\phi_f$) for the NBB case.
industrial systems. For instance, this combustion is beneficial in furnaces or kilns of the process industry such as cement, glass and steel, etc., where combustion releasing heat transfers to the target internally, rather than through the furnace wall (of, e.g., water tubes). In these applications, uniform temperature distribution in the furnace is favorable for the heat treatment or melting procedures. Potentially, this combustion technology can also be utilized in stationary gas turbines and diesel engines, where combustion is initiated by auto-ignition. By using this technology, high thermal efficiency, low acoustic oscillations and low NOx emissions will be achieved in these compact power or propulsion equipment. Nevertheless, such applications are still not in reality due to the difficulties of meeting all the engine requirements when operating in the MILD regime. Besides, the MILD combustion should be very suitable for the utilization of wastes (industrial, agricultural and domestic wastes) and low calorific value fuels, like biogas, coke oven gas, blast furnace gas, etc. Problems of flame instability and quenching in traditional combustion are unlikely to occur in MILD combustion. In addition, this technology may be adopted in the steam reforming of hydrocarbon fuels, since the distributed reactions and uniform temperature and composition fields are favorable for producing CO and hydrogen efficiently. On the other hand, it should be noted that, when designing MILD combustion furnaces, to gain a sufficiently high jet velocity and momentum, small nozzle diameters should be considered where possible. Rational nozzle arrangement and burner position are also important for tardy ignition of the combustible mixture as well as avoiding locally reaching high temperatures. Moreover, the furnace size could be considered smaller than that in traditional combustion because of elevated heat transfer rate, but the optimum furnace type (furnace length, width and height) should be adopted to guarantee the internal exhaust gas recirculation (EGR) conditions. Also, importantly, convective and radiative heat transfer on the wall or in the furnace should be seriously considered to keep the wall temperature higher than the auto-ignition temperature, since hot flue gas or hot wall is crucial for the spontaneous ignition of incoming reactants.

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